Calculation method - Cooling connections

Suction line

The following table lists recommendations for each suction line based on the minimum and maximum cooling capacity.

Evap. temp. °C		GAS LINE EVAPORATOR SUCTION COMPRESSOR R-449A / R-452A / R-404A							GAS LINE EVAPORATOR SUCTION COMPRESSOR R-134a										
	Diameter line	Minimum Cooling	Cooling capacity max. (kW) for a temperature drop of saturation 1 K, as equivalent to length of line					Minimum Cooling	Cooling capacity max. (kW) for a temperature drop of saturation 1 K, as equivalent to length of line										
		capacity (kW)								capacity (kW)	10 m	15 m	20 m	25 m	30 m	40 m	50 m		
	3/8"	0.2	1.3	1.0	0.9	0.8	0.7	0.6	0.5	0.2	0.8	0.7	0.6	0.5	0.4	0.4	0.3		
	1/2"	0.5	3.2	2.6	2.2	1.9	1.7	1.5	1.3	0.5	2.0	1.6	1.4	1.2	1.1	0.9	0.8		
	5/8"	0.9	6.1	4.9	4.2	3.7	3.3	2.8	2.5	0.9	3.8	3.1	2.6	2.3	2.1	1.8	1.6		
High temperature ration temperature: 0 °C	3/4"	1.4	10.1	8.1	6.9	6.1	5.5	4.7	4.2	1.5	6.4	5.1	4.4	3.9	3.5	3.0	2.6		
	7/8"	2.0	15.8	13	11	9.6	8.7	7.4	6.5	2.2	10	8.0	6.9	6.1	5.5	4.7	4.1		
	1"	3.0	22	19	16	14	13	11	9.6	3.2	15	12	10.0	8.9	8.0	6.9	6.1		
	1 1/8 "	4.0	28	25	22	19	17	15	13	3.7	17	16	14	12	11	9.4	8.3		
	1 3/8 "	7	41	41	36	32	29	25	22	6	24	24	23	21	19	16	14		
	1 5/8 "	10	58	58	58	52	47	40	35	9	35	35	35	33	30	25	23		
ap o	2 1/8	21	103	103	103	103	99	145	/5	19	01	01	01	01	05	54	48		
Ĕ	2 3/0	55	100	225	100	100	100	145	200	50	125	125	95	125	95	95	122		
	3 5/8 "	80	300	300	300	300	300	300	300	75	180	180	180	135	180	180	133		
	4 1/8 "	115	400	400	400	400	400	400	400	100	230	230	230	230	230	230	230		
	3/8"	0.2	0.9	0.7	0.6	0.5	0.5	0.4	0.4	0.2	0.55	0.44	0.37	0.33	0.30	0.25	0.22		
	1/2"	0.4	2.2	1.8	1.5	1.3	1.2	1.0	0.9	0.4	1.3	1.1	0.9	0.8	0.7	0.6	0.5		
srature iture: -10 °C	5/8"	0.8	4.2	3.4	2.9	2.5	2.3	2.0	1.7	0.7	2.6	2.1	1.8	1.5	1.4	1.2	1.1		
	3/4"	1.2	7.0	5.6	4.8	4.3	3.9	3.3	2.9	1.2	4.3	3.4	2.9	2.6	2.3	2.0	1.8		
	7/8"	1.7	11	8.8	7.5	6.7	6.0	5.1	4.5	1.8	6.7	5.4	4.6	4.1	3.7	3.1	2.8		
	1"	2.5	15	13	11	9.7	8.8	7.5	6.7	2.6	9.9	7.9	6.7	6.0	5.4	4.6	4.1		
mpe	1 1/8 "	3.5	19	18	15	13	12	10	9.1	3.0	11	10.8	9.2	8.1	7.4	6.3	5.5		
e te tem	1 3/8 "	5.5	28	28	25	22	20	17	15	5.0	16	17	16	14	12	11	9.4		
sitiv	1 5/8 "	9.0	40	40	40	36	33	28	25	7.5	23	24	25	22	20	17	15		
Pos	2 1/8 "	18	70	70	70	70	69	59	52	15	41	42	43	44	42	36	32		
vapi	2 5/8 "	30	105	105	105	105	105	101	90	25	62	63	64	65	66	62	55		
ш	3 1/8 "	50	155	155	155	155	155	155	146	40	90	91	92	93	94	95	89.7		
	3 5/8 "	65	200	200	200	200	200	200	200	60	120	121	122	123	124	125	126		
	4 1/8 "	90	265	265	265	265	265	265	265	75	150	151	152	153	154	155	156		
	3/8"	0.2	0.4	0.3	0.3	0.2	0.2	0.2	0.2										
	1/2"	0.3	1.0	0.8	0.7	0.6	0.5	0.4	0.4			Suction pipe selection							
S	5/8 2/4"	0.5	1.8	1.5	1.3	1.1	1.0	0.9	0.8			Given a co	oling capaci	ty at a deter	mined evapo	orating temp	erature, it is		
-30	5/4 7/8"	1.2	3.1	2.5	2.1	20	26	1.4	2.0			the minim	um recomn	nended valu	iciddes this le for the p	ipe and th	e maximum		
ratu ture:	1"	1.2	6.2	5.5	4.8	43	3.0	33	2.0			recommen	ded value d	lepending or	n the equiva	lent length	of the pipe.		
npe	11/8"	2.0	8.1	7.7	6.6	5.8	5.3	4.5	4.0			To ensure	the correct	oil return in	vertical uprig	ghts, it is re	commended		
emp	1 3/8 "	3.5	12	12	11	9.9	8.9	7.6	6.7			to select a pipe diameter where the cooling capacity is 50 % higher than the minimum recommended value. It is recommended to avoid the selection of pipes with red data, which are associated with a cooling performance loss of more than 15 %.							
ative on t	1 5/8 "	5.5	17	17	17	16	14	12	11										
Neg orati	2 1/8 "	11	30	30	30	30	30	26	23										
vapo	2 5/8 "	18	46	46	46	46	46	45	39										
ú	3 1/8 "	30	66	66	66	66	66	66	64			associated with a maximum das velocity of 15 m/s							
	3 5/8 "	45	90	90	90	90	90	90	90						,				
	4 1/8 "	60	115	115	115	115	115	115	115			Pipe insula	tion						
	3/8"	0.2	0.7	0.5	0.4	0.4	0.4	0.3	0.3			in suction	n pipes, ti nended in	he followin elastomeric	foam in o	n insulation Inder to av	n thickness oid surface		
ы	1/2"	0.5	1.6	1.3	1.1	1.0	0.9	0.7	0.7			condensation at an ambient temperature of 25 °C and 50 % RH: High and positive temperature: 10 mm							
erature - Vapour injectic n temperature: -30 °C	5/8"	0.8	3.1	2.5	2.1	1.9	1.7	1.4	1.3										
	3/4"	1.3	5.1	4.1	3.5	3.1	2.8	2.4	2.1			Negative temperature (Evap. temp.: -30 °C): 20 mm							
	7/8"	1.8	8.0	6.4	5.5	4.9	4.4	3.7	3.3			Calculation	n basis						
	1"	2.5	11	9.4	8.0	7.1	6.4	5.5	4.9			This calculation method developed by INTARCON is provided fo guidance only and it is the responsibility of the designer to carry out the appropriate checks. The calculation is only valid for the pre dimensioning of refrigerant lines in copper piping for refrigeration use The maximum cooling capacities indicated for each case correspond							
	1 1/8 "	4.0	14	13	11	9.7	8.8	7.5	6.6										
	1 3/8 "	6.0	20	20	19	16	15	13	11										
atior	15/8"	10	30	30	30	26	24	20	18										
ve te	2 1/8	30.0	75	50	50	50	50	43	86 66			to a press	sure drop o	of 1 K at s	aturation te	mperature,	with a gas		
gativ Eva	2 3/0	50.0	110	110	110	110	110	110	110			velocity lir	nit of 15 m	/s (data in b	lue).		under Pr		
Ne	3 5/8 "	70.0	150	150	150	150	150	150	150			correspond	um recomn to a mini	mum veloci	ing capacitient of 4 m/	es for the s s at mediu	m and high		
	4 1 /0 "	100.0	200	200	200	200	200	200	200			temperatu	re. 5 m/s at	low temper	ature		2.10 mgn		

All data ratings have been calculated based on a condensing temperature of 45 °C, evaporator superheat of 10 K and expansion valve subcooling of 0 K or 40 K for liquid subcooled at low temperature.

Fluid line

The following table indicates the recommended average cooling capacity for fluid piping and refrigerant charge according to the diameter.

		Co	oling capacity recom					
	Diameter copper	Without s	subcooling	With sul	bcooling 0°C	Refrigerant load (gr/m)		
	inite	R-404A / R-452A	R-134a / R-449A	R-404A	R-134a / R-449A	R-449A / R-452A	R-134a / R-449A	
	1/4"	2	3	4	5	20	25	
	3/8"	5	7	12	15	50	65	
	1/2"	10	14	24	30	100	120	
	5/8"	15	23	40	50	160	200	
	3/4"	23	35	55	80	240	300	
	7/8"	32	50	80	120	340	400	
	1"	43	63	105	150	450	500	
	1 1/8 "	55	80	135	200	550	700	
	1 3/8 "	80	120	200	300	850	1 000	
	1 5/8 "	115	170	280	400	1 200	1 500	
	2 1/8 "	200	300	500	700	2 100	2 500	

Equivalent length

The equivalent length of a cooling line is usually between 1.2 and 5 times the actual length depending on the number of elbows and reductions. A rough estimate can be made using the values indicated in the following table:

Diamatar	Longitud equivalente (m)									
cooper line	Elbow to 90°	T-branch Straight flow Derived flow		Reduction	Siphon	Service angular valve	Gate service valve			
3/8"	0.7	0.3	0.8	0.3	1.1	1.8	0.2			
1/2"	0.8	0.3	0.9	0.4	1.2	2.0	0.2			
5/8"	0.9	0.4	1.0	0.5	1.4	2.2	0.3			
3/4"	1.0	0.4	1.2	0.6	1.6	2.5	0.3			
7/8"	1.1	0.5	1.4	0.6	1.8	3.0	0.3			
1"	1.2	0.5	1.5	0.7	2.0	3.5	0.3			
1 1/8 "	1.4	0.6	1.8	0.8	2.3	4.0	0.4			
1 3/8 "	1.7	0.7	2.2	1.0	2.7	5.0	0.5			
1 5/8 "	2.0	0.9	2.7	1.2	3.5	6.0	0.6			
2 1/8 "	2.5	1.1	3.3	1.5	4.3	8.0	0.7			

Recommendations

In designing the layout of the refrigerant lines the following practices are recommended:

- Design the layout as straight as possible, with the minimum number of elbows, diversions and valves.
- Install a trap in vertical runs of suction line every 3 meters.
- Install the horizontal sections of the suction line in a downward slope towards the compressor.
- Evaporators refrigeration connections to the intake manifold must always be conducted through the top of the units.

Example - Refrigeration line calculation



Liquid piping selection

Given a given cooling capacity at a given evaporating temperature, the liquid pipe diameter must be selected according to the recommended cooling capacity with a range of \pm 50 %.

It is recommended that liquid piping should not be insulated unless it is exposed to direct sunlight or in twostage compression or vapour injection systems, where the piping should be insulated with a minimum 10 mm thick element to preserve liquid subcooling and prevent surface condensation.

The recommended cooling capacities for liquid lines correspond to flow rates of 1 m/s.

Calculation example

Dimensioning of refrigerant lines according to service to a 1500 W evaporator for low temperature cold rooms at -20 $^{\circ}\text{C}$ with a DT1 of 7 K.

The liquid line is dimensioned based on the recommended cooling capacity, $1/4^{\prime\prime}$ piping being admissible.

Initially we take an equivalent length of 1.5 times the actual length. This is: Leq = $1.5 \times 20 \text{ m} = 30 \text{ m}.$

Admitting in the suction line a pressure drop equivalent to 1K saturation temperature, if we go to the column for 30 m of low temperature pipe (-30 °C evaporation), finding that:

Pipe 3/4" pipe has a recommended maximum power of 1.7 kW, but with a loss of efficiency greater than 15 $\,\%$ (figures in red).

Pipe 7/8" has a minimum power of 1.5 kW, impeding the return of gas in vertical uprights.

 $7/8^{\prime\prime}$ diameter it is recommended for horizontal and descending sections, and $3/4^{\prime\prime}$ diameter only in vertical uprights.

We can see that the estimate of the equivalent length is correct:

Leq = 20 m + 3x 1.1 m (elbow) + 2x 1.6 m (oil trap) + 2.5 m (check valve) = 29 m